

# Newly developed H<sub>2</sub> Generator using Highly-Oxygen-Permeable Ceria-based Membrane

Prof. Hiroshi TAKAMURA (Tohoku Univ.)

## 1. Advantages of MPOX (Partial Oxidation of Methane by using Oxygen Permeable Membranes)

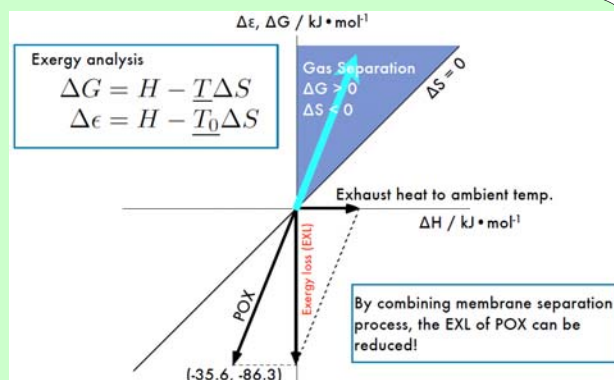
- Objective : Hydrogen generation from natural gas
- Comparison of candidate reaction

	Reaction Formula	$\Delta G^0_{298}$ (kJ/mol)	$\Delta H^0_{298}$ (kJ/mol)	$\Delta S^0_{298}$ (kJ/mol)	drawbacks
Steam reforming	$\text{CH}_4 + \text{H}_2\text{O} \rightarrow \text{CO} + 3\text{H}_2$	150.843	250.176 (endothermic)	333.164	Slow Start-Ups: Approx. 1h
Partial oxidation	$\text{CH}_4 + 1/2\text{O}_2 \rightarrow \text{CO} + 2\text{H}_2$	-86.347	-35.654 (exothermic)	170.024	Large Exergy Loss

- Partial Oxidation of Methane (POX)  
Can Large Exergy loss (EXL) of POX be reduced?

**Exergy Analysis**  
Combination with the reaction with exergy vector having opposite direction to POX is promising.

- MPOX : Membrane separation process + POX ( $\Delta G > 0, \Delta S < 0$ )
- Reduction of EXL of POX is achieved.



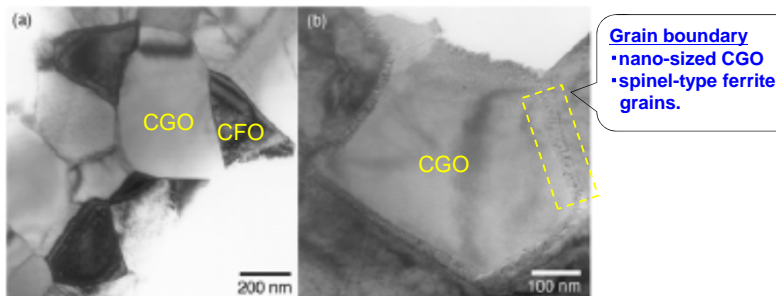
Exergy Analysis shows the advantage of MPOX (POX+ Gas Separation)



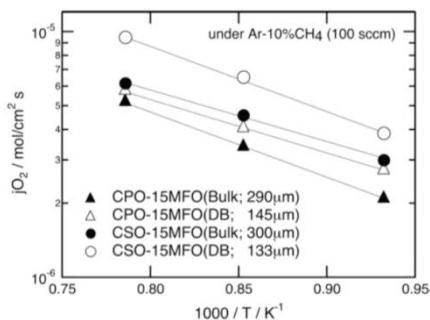
MPOX effectively utilizes the free energy generated from partial oxidation reaction to Oxygen separation

## 2. Ceria-based oxygen permeable membranes

	Composition	Oxygen flux density $\mu\text{mol} \cdot \text{cm}^{-2} \cdot \text{s}^{-1}$	Temp. °C	Ref.
BSCF	$\text{Ba}_{0.5}\text{Sr}_{0.5}\text{Co}_{0.8}\text{Fe}_{0.2}\text{O}_3$	8.6	875	Shao <i>et al.</i> , 2001
LSGF	$\text{La}_{0.7}\text{Sr}_{0.3}\text{Ga}_{0.6}\text{Fe}_{0.4}\text{O}_3$	8.2	1000	Ishihara <i>et al.</i> , 2002
PSAF	$\text{Pr}_{0.7}\text{Sr}_{0.3}\text{Fe}_{0.8}\text{Al}_{0.2}\text{O}_3$	8.2	1000	Takamura <i>et al.</i> , 2002
Ceria-MFO	$(\text{Ce}, \text{Sm})\text{O}_{2-15}\text{vol}\%\text{MnFe}_2\text{O}_4$	10.0	1000	Takamura <i>et al.</i> , 2002
LBSFI	$(\text{La}_{0.5}\text{Ba}_{0.5}\text{Sr}_{0.2})(\text{Fe}_{0.6}\text{In}_{0.4})\text{O}_3$	10.6	1000	Aizumi <i>et al.</i> , 2004



Ceria-MFO:  $(\text{Ce}, \text{Gd})\text{O}_{2-17}\text{vol}\%\text{CoFe}_2\text{O}_4$  fired at 1300°C for 2 h



CSO membrane made by tape-casting technique: 5cm x 5cm

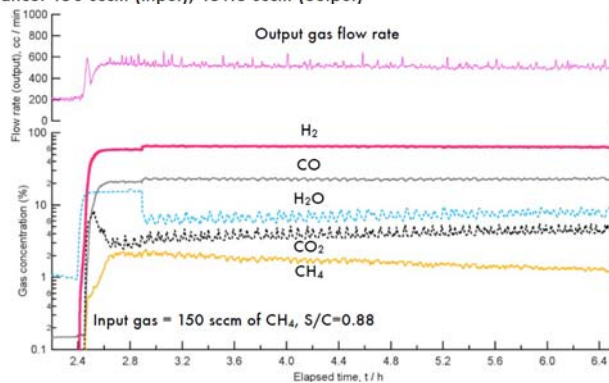
Oxygen permeation properties

- Ceria-MFO:  $(\text{Ce}, \text{Re})\text{O}_2 + \text{MeFe}_2\text{O}_4$
- $(\text{Ce}, \text{Re})\text{O}_2$  : Oxygen Conductive Phase (Re is an acceptor) (CGO (Re=Gd), CSO (Re=Sm) and CPO (Re=Pr))
- $\text{MeFe}_2\text{O}_4$  : Electron Conductive Phase

## 3. Characteristics of MPOX reformer

No. of modules	CH <sub>4</sub> (sccm)	Air (sccm)	Temp. (°C)	S/C	$j_{\text{O}_2}$ ( $\mu\text{mol}/\text{cm}^2 \cdot \text{s}$ )	CH <sub>4</sub> conv. (%)	CO selectivity (%)	H <sub>2</sub> selectivity (%)
1	150	500	780	0.88	3.3	96	84	89

\*C-balance: 150 sccm (input); 151.8 sccm (output)



Flow rate and composition of reformat gas



MPOX reformer module comprising of CSO.15MFO and ZMG232R (left) and its 20 stacks (right)

To produce 10 liter/min of hydrogen, stack of 20 modules is required.

## 4. Patent available for licensing

Patent No. : WO2003/084894, WO2007/046314 (JP, US, EP)

Contact : Takuji OHINATA (JST)  
phone: +81-3-5214-8486, e-mail: license@jst.go.jp